

PROCESS DYNAMICS AND CONTROL

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RECAP

- ◉ Control Instrumentation

OUTLINE

- Stability of dynamic systems
- Closed-loop stability
- Closed-loop transfer functions
 - Block diagram representation
- Stability analysis methods
 - Root locus
 - Bode method

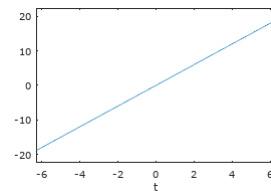
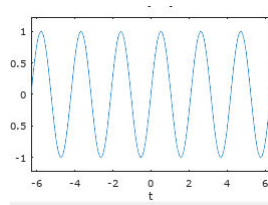
Seborg's book 3rd ed (Int'l ed): Chapter 10
 Nikazar's book: Chapters 6, 8, 9, 10.

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STABILITY OF DYNAMIC SYSTEMS

Bounded-input bounded-output (BIBO) stability

- **Definition:** with all **inputs bounded**, all **outputs** must be **bounded**.
 - sine input
 - Step input
 - Ramp input?



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UNBOUNDED PROCESS OUTPUT

- ◉ Unbounded process variables hit a **physical limitation** (they do not go to infinity!)

- **Examples**

- Tank overflow
- Explosion
- Vessels burst
- Product degradation
- ...

These are serious consequences!

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STABILITY VS. GOOD OPERATION

- ◉ Stability is a **minimum** requirement for control performance.
- ◉ A **stable** system can have a **poor operation** (or **control performance**)

- **Example:**

Reactor with **step increase of 1 C** in inlet temperature



Steady-state increase of **100 C** in outlet temperature!

Stable but very sensitive

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STABILITY OF LINEAR DYNAMIC SYSTEMS

- General form of a linear dynamic system

$$\frac{d^n Y}{dt^n} + a_1 \frac{d^{n-1} Y}{dt^{n-1}} + \dots + a_n Y = \cancel{f(t)} \leftarrow \begin{array}{l} \text{Ignore input} \\ \text{(assuming} \\ \text{bounded)} \end{array}$$

- Laplace transform (zero initial conditions)

$$(s^n + a_{n-1}s^{n-1} + \dots + a_1s + a_0)Y(s) = 0$$

- Inverse Laplace

Thomas marlin's Process Control book

$$Y(t) = A_1 e^{\alpha_1 t} + \dots + (B_1 + B_2 t + \dots) e^{\alpha_p t} \\ + \dots + [C_1 \cos(\omega t) + C_2 \sin(\omega t)] e^{\alpha_q t} + \dots$$

All exponents (α) must be negative for BIBO stability

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STABILITY OF LINEAR DYNAMIC SYSTEMS

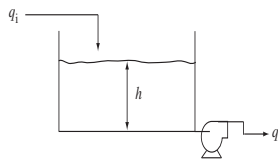
- Example 1

$$\frac{d^2 T'}{dt^2} - 1.23 \frac{dT'}{dt} - 1.38 T' = 0$$

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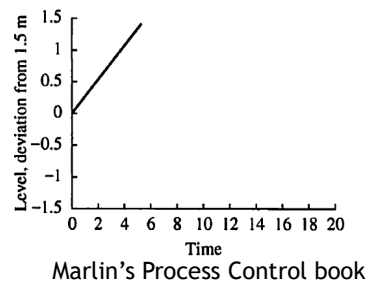
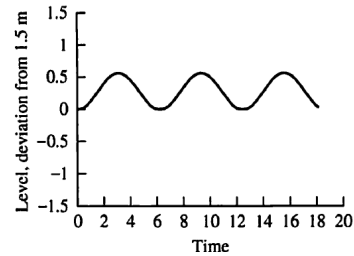
STABILITY OF LINEAR DYNAMIC SYSTEMS

Example 2



- Sine response
 - Stable
- Step response
 - Unstable

Why different behaviors?



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SOME REMARKS

- By definition, a stable system must have **bounded output** for all types of bounded inputs.
- Almost all processes have **nonlinear** dynamics
 - Use linearized model
 - Local stability (around steady state)
 - Valid only near **linearization point**.

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LOCATION OF ROOTS AND STABILITY

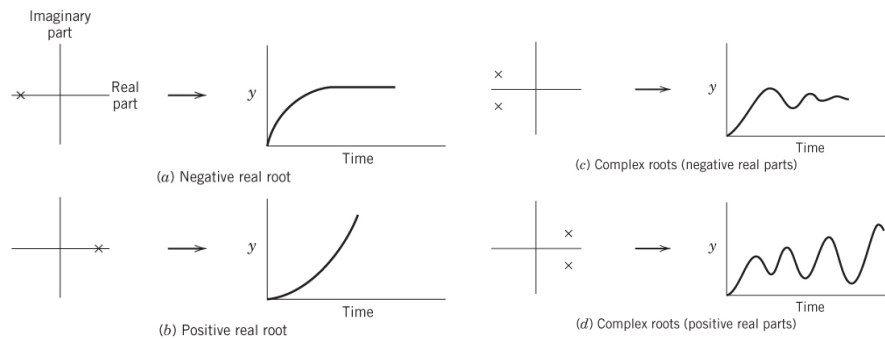


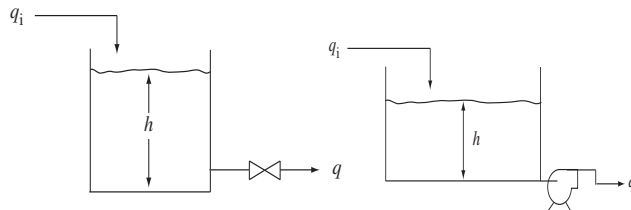
Figure 11.26 Contributions of characteristic equation roots to closed-loop response.

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OPEN-LOOP VS. CLOSED-LOOP STABILITY

- **Open-loop stability:** stability **without** controller
- **Closed-loop stability:** stability **with** controller

Examples



Importance of closed-loop stability

- ✓ Stability of control designs
- ✓ Tuning of controllers
- ✓ Analysis of control performance

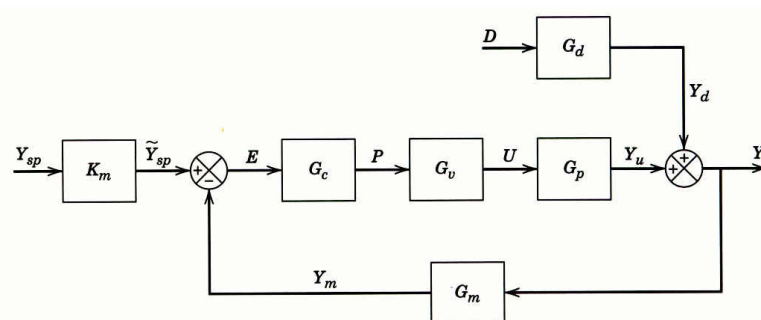
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STABILITY OF CLOSED-LOOP SYSTEMS

- Analyze the overall transfer function for stability
- Can a system with a controller go **unstable**?

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STANDARD CLOSED-LOOP BLOCK DIAGRAM



Seborg's et al. Process Dynamics and Control book

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